

# Fuel-Neutral Studies of Particulate Matter Transport Emissions

P.I.: Mark Stewart

Pacific Northwest National Laboratory

June 9, 2016

Project ID: ACE056

This presentation does not contain any proprietary, confidential, or otherwise restricted information



#### PNNL

Alla Zelenyuk, David Bell, Chaitanya Sampara

#### **GM**

Kushal Naranayaswamy, Paul Najt, Arun Solomon, Wei Li

University of Wisconsin Engine Research Center

David Rothamer, Christopher Rutland, Sandeep Viswanathan, Jonathan Molina, Andrea Shen, Yangdongfang Yang, Mike Andrie, Todd Fansler

Program Managers: Ken Howden and Gurpreet Singh

This work was funded by the U.S. Department of Energy (DOE) Vehicle Technologies Program

#### **Timeline**

- Start FY09
- Finish FY17

#### **Budget**

- Funding received in FY15 - \$200K
- ► Planned budget for FY16 \$250K

#### **Barriers**

- Barriers addressed for enabling of high-efficiency engine technology:
  - B.\* Lack of cost-effective emission control
  - C.\* Lack of modeling capability for combustion and emission control
  - F.\* Lack of actual emissions data on pre-commercial and future combustion engines

#### **Partners**

- General Motors Company provide project guidance, support for ERC
- Engine Research Center at University of Wisconsin, Madison
   host and operate test engines, perform experiments

<sup>\*</sup> Indexed to list in VTO Multi-Year Program Plan

### Relevance and objectives



Proudly Operated by Battelle Since 1965

Overall objective: Enable adoption of future high-efficiency engine technologies

Barrier: Lack of actual emissions data on precommercial and future combustion engines Objective: Comprehensive particulate characterization with single-cylinder test engines, guided by industry



2016 Chevy Cruze with 1.4 L turbocharged DI LE2 engine By Ryan Hildebrand - Own work, CC BY-SA 4.0, https://commons.wikimedia.org/w/index.php?curid=46673960

Barrier: Lack of cost-effective emission control

Objective: Seek to shorten development time of filtration technologies for future engines by improving fundamental understanding of how filter media properties impact backpressure and filtration efficiency

and

Barrier: Lack of modeling capability for combustion and emission control

Objective: Develop modeling approaches relevant to the likely key challenge for SIDI filtration – high number efficiency at high exhaust temperatures (implying little soot accumulation in filters)

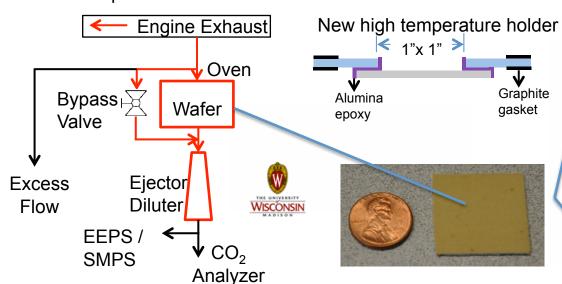
#### **Approach**

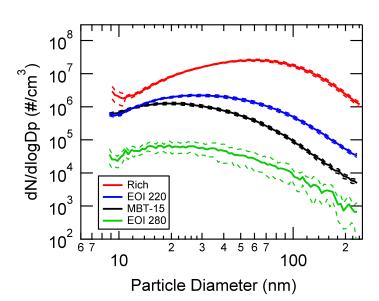
### **Experiments**

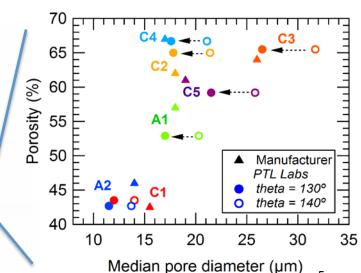


Proudly Operated by Battelle Since 1965

- Three extensive cooperative experimental campaigns have been carried out at the University of Wisconsin Engine Research Center
  - Characterization of exhaust particulates over a wide range of fuels and operating conditions
  - Fundamental studies around soot formation
- EFA filtration experiments
  - Wide variety of filters and particulate populations
  - Current focus is low (but non-zero) soot loadings
  - Refinements in materials and methods (scan rates, etc.)
  - New high-temperature holder simulates close-coupled filter placement







(theta = assumed Hg contact angle)

#### **Approach**

### Filter characterization and modeling



Proudly Operated by Battelle Since 1965

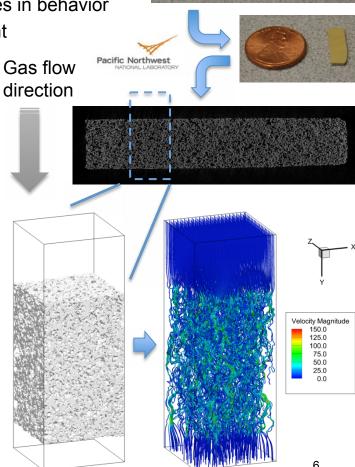
- Detailed characterization of filter substrates
  - Hg porosimetry, permeability, exploring other methods
  - Micro X-Ray CT
    - Porosimetry pore sizes do not account for all differences in behavior
    - Differences in texture, microstructure are also important
- Goal is improved device-scale filter models
  - Demonstrated improved clean filter efficiency predictions over baseline unit collector model with modified diffusion capture and U of Wisconsin Heterogeneous Multi-scale Filtration (HMF) model
  - Experiments show that even very small accumulations of soot and ash affect capture efficiency and backpressure

WISCONSIN

 Currently seeking general models that require minimum tuning for performance predictions with various substrates, particle size distributions, filter loadings



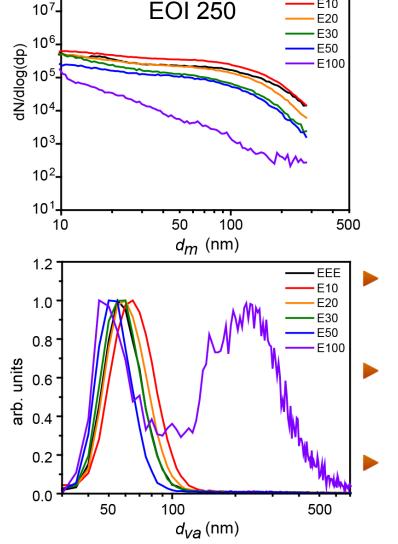




#### Technical accomplishments - Shown at 2015 AMR **Particulate characterization**



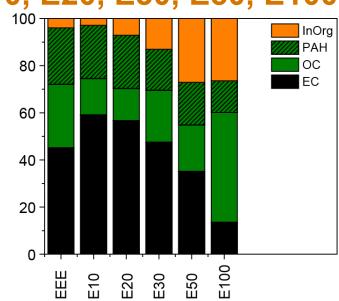
DI PM for different fuel blends: EEE, E10, E20, E30, E50, E100



10<sup>7</sup>-

Average compositions of fractal particles

InOrg = inorganics PAH = polycyclic aromatic hydrocarbons OC = organic carbon EC = inorganic carbon



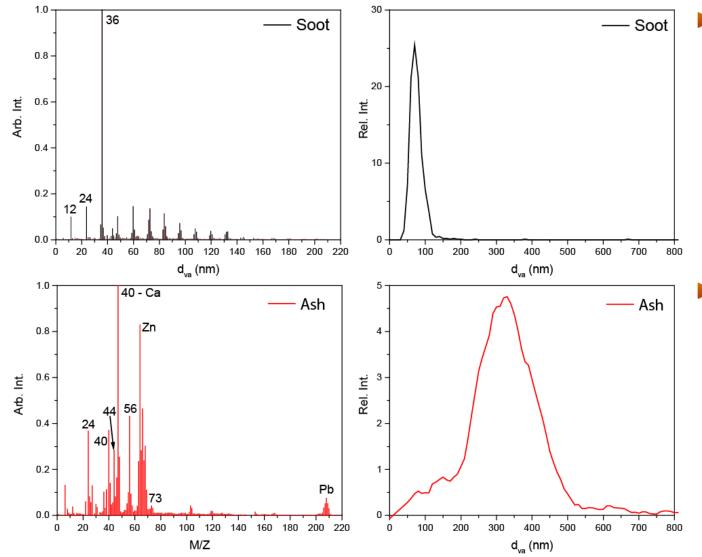
- The vast majority of particles emitted by SIDI engine under all engine operating conditions and fuel blends (except E100) are fractal soot agglomerates
- The average diameter of primary spherules that comprise fractal soot agglomerates varies depending on fuel and engine operating condition
- Fractal soot agglomerates have high organic content, which varies between 40 and 60%, depending on fuel and engine operating condition

# Technical accomplishments Particulate characterization



Proudly Operated by Battelle Since 1965

#### Composition of *individual* exhaust particles



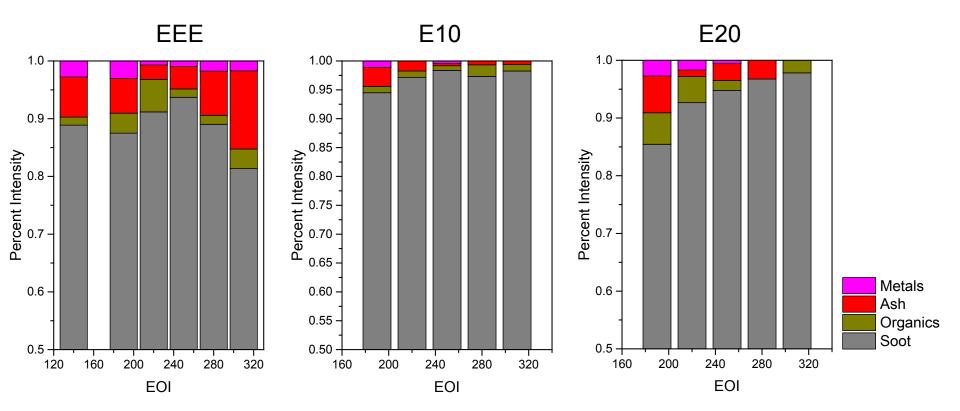
- Exhaust PM represents a complex mixture of particles with various sizes, compositions, morphologies, and shapes
- Examples: fractal soot particles and compact ash particles with larger vacuum aerodynamic diameter (d<sub>va</sub>)

# Technical accomplishments Particulate characterization



#### Single particle analysis for different fuels: EEE, E10, E20

- Fraction of different particle types depends on engine operating condition and fuel
- Note that the plots below only show range from 0.5 (50%) to 1 (100%), since Soot represent the dominant particle type for these conditions and it is difficult to see the contribution from other particle types



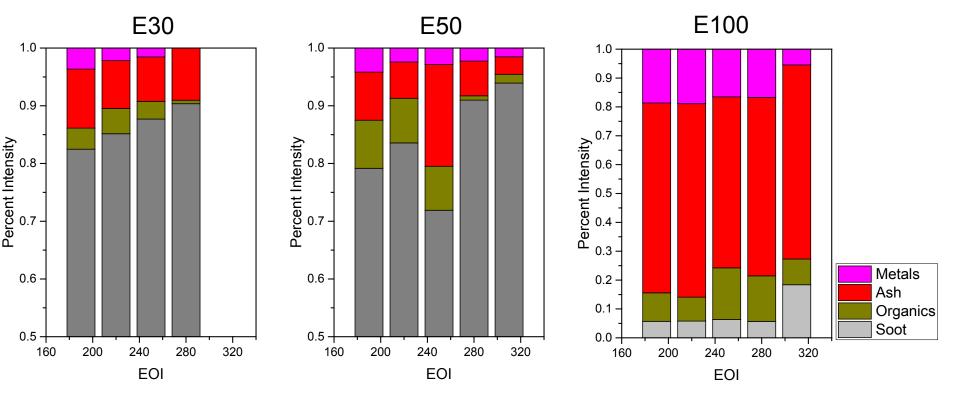
# Technical accomplishments Particulate characterization



Proudly Operated by Battelle Since 1965

#### Single particle analysis for different fuels: E30, E50, E100

- Fraction of different particle types depends on engine operating condition and fuel
- Note that the first two plots only show range from 0.5 (50%) to 1 (100%), while the plot for E100 starts at 0
- ► E100 produces significantly fewer soot particulates. As a result, larger non-fractal particles (ash particles, engine wear & tear) represent significant fraction

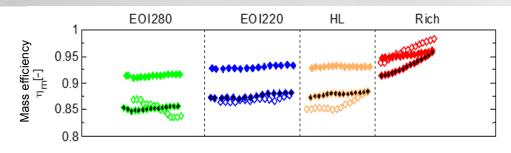


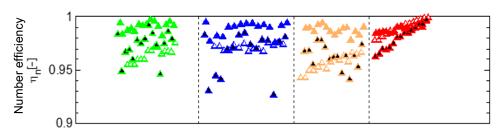
# Technical accomplishments Device-scale modeling

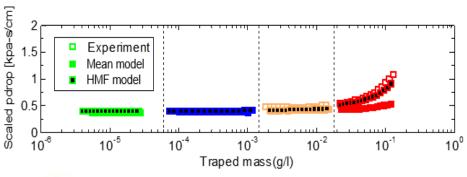


Proudly Operated by Battelle Since 1965

- Standard single unit collector filtration model\* and U of Wisc HMF model predictions were compared to new filtration data
- Parameters such as soot deposit porosity in the wall and 'percolation factor' are typically tuned for a specific filter, engine
- Hard to find a model and set of parameters that works well for:
  - Mass efficiency
  - Number efficiency
  - Pressure drop
     under various different engine
     operating conditions even for a single filter substrate









Filter sample: C1-60 Face velocity: 2.5 cm/s

Filtration temperature: 125 C

<sup>\*</sup> Konstandopoulos, A. G. and Johnson, J. H., "Wall-Flow Diesel Particulate Filters — Their Pressure Drop and Collection Efficiency," SAE Tech. Pap. 890405, 1989.



Proudly Operated by Battelle Since 1965

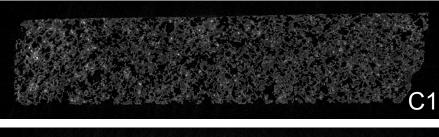
Have obtained a large volume of high quality, repeatable filtration data for a range of substrates, conditions

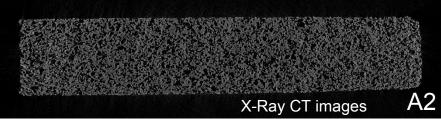
#### **Example Study: C1 versus A2**

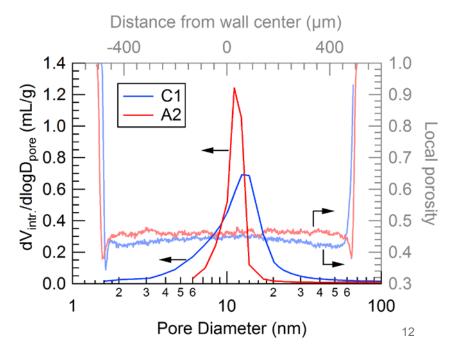
C1 and A2 have similar:

- Pore size
- Total porosity
- Porosity across wall thickness but differ in:
- Material (Cordierite vs. Aluminum Titanate)
- Width of pore size distribution (W)
- Clean permeability (~12% difference)

Batch	Por. (%)	MPD (μm)	$\sigma_{\mu m}^{}$	W	Th. (mm)	Perm. *10 <sup>-13</sup> (m <sup>2</sup> )	
C1	43	12	4.3	0.55	1.05	6.8±0.1	
A2	43	11.4	8.0	0.24	1.05	7.6±0.1	









Proudly Operated by Battelle Since 1965

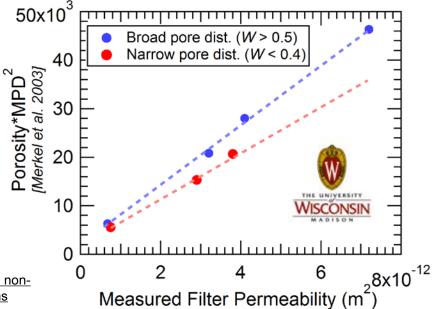
Batch	MPD (μm)	σ <sub>log-</sub>	W	
<b>C1</b>	12	0.31	0.55	
C2	17.9	0.19	0.55	
<b>C3</b>	26.6	0.20	0.52	
C4	17.6	0.13	0.36	
<b>C5</b>	21.75	0.18	0.49	
A1	17	0.15	0.39	
A2	11.4	0.1	0.24	

- Merkel et al.\* proposed the "W" metric for width of pore size distribution and related it to loaded backpressure
- Size distribution width metrics are shown here for eight of the substrates included in this study
- Clean permeability seems to depend on W as well as porosity and pore size
- Lower W has been associated with better pore connectivity

MPD = median pore diameter

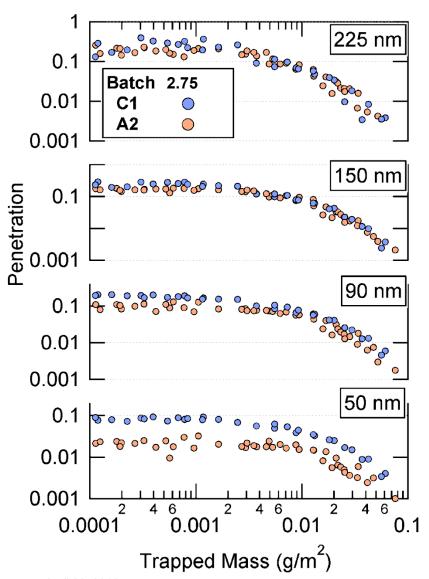
$$W = \frac{d_{50} - d_{10}}{d_{50}}$$

Clean permeability ∝ Porosity · MPD²



<sup>\*</sup> Merkel, G. A., W. A. Cutler, T. Tao, A. Chiffey, P. Phillips, M. V. Twigg and A. Walker (2003). New cordierite diesel particulate filters for catalyzed and non-catalyzed applications. 9th Diesel Engine Emissions Reduction Conference, Newport, Rhode Island.





- Penetration of large particles similar
  - Likely dominated by interception
- Significant difference in penetration of small particles
  - Likely dominated by diffusion
  - Better pore connectivity in A2 could contribute to higher efficiency through:
    - Lower interstitial velocities
    - More uniform access of flowing gas to internal surface area

Filter substrates: C1, A2
Face velocity: 2.75 cm/s

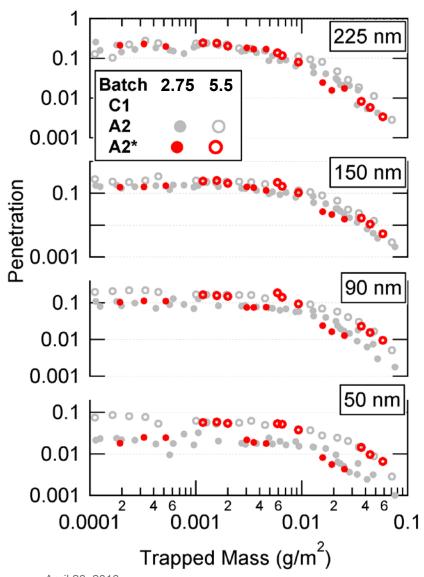
Filtration temperature: 125 C



14

April 26, 2016





- Checked impact of sample to sample variability - trends still consistent across multiple samples
- Changing velocity had little impact on removal of large particles
  - Consistent with theory interception term has no velocity dependence
- Changing velocity had significant impact on removal of small particles
  - Trend again consistent with theory

Filter substrate: A2

Face velocities: 2.75, 5.5 cm/s

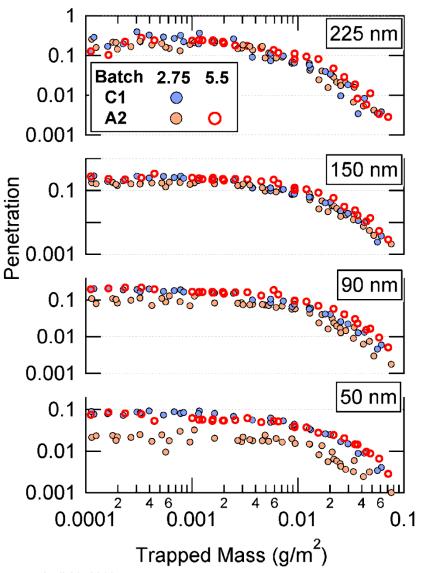
Filtration temperature: 125 C



15

April 26, 2016





- A2 performance for removal of small particles equals that of C1 at half the filtration velocity
- Since back-pressures are comparable, A2 would seem to have a clear advantage
- Consistent with longstanding consensus that narrow particle size distribution is better
- Little difference in performance for large particles

Filter substrates: C1, A2

Face velocities: 2.75, 5.5 cm/s

Filtration temperature: 125 C



April 26, 2016 16

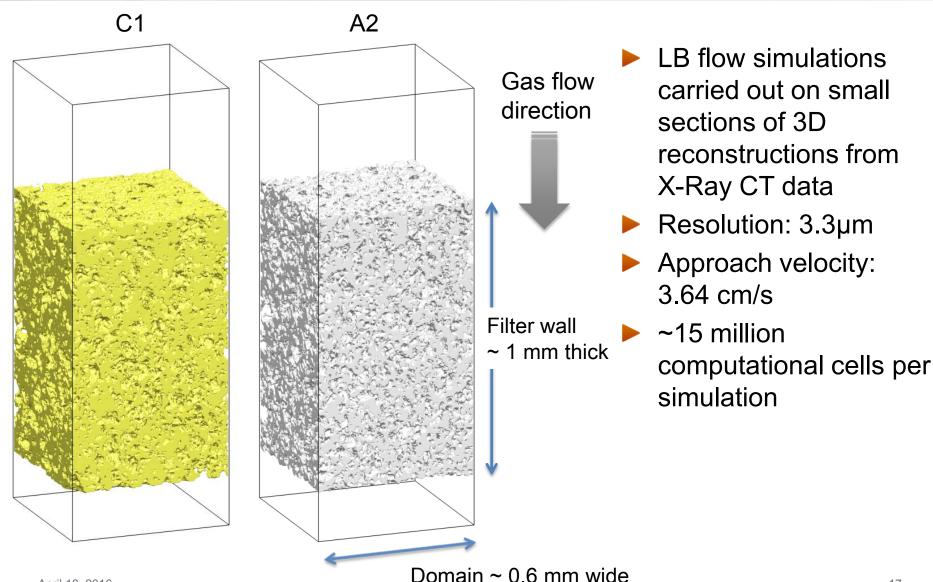
#### **Technical accomplishments**

### **Lattice Boltzmann simulations**



Proudly Operated by Battelle Since 1965

17

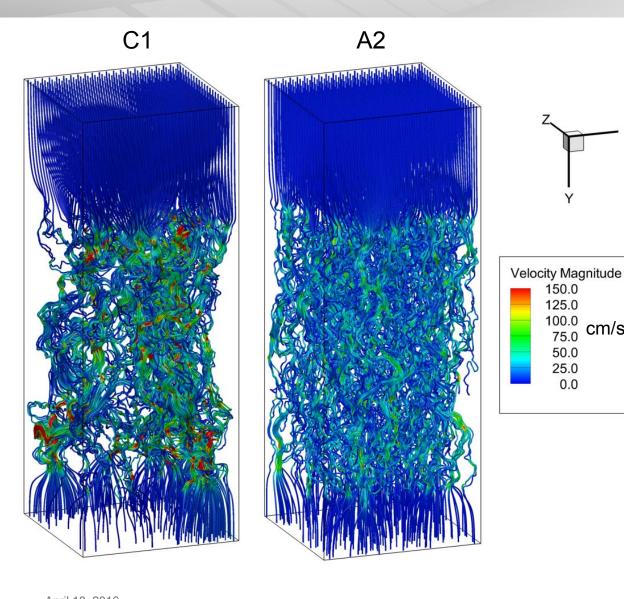


#### **Technical accomplishments**

#### **Lattice Boltzmann simulations**



Proudly Operated by Battelle Since 1965



- Streamlines colored according to local velocity
  - Fewer major flow paths per volume through C1
- Higher local velocity in bottlenecks
- Better flow distribution in A2 gives the exhaust access to more surface area for capture by diffusion
- Lower velocities also mean longer residence times in the wall

April 18, 2016 18

150.0 125.0

100.0

50.0 25.0

0.0

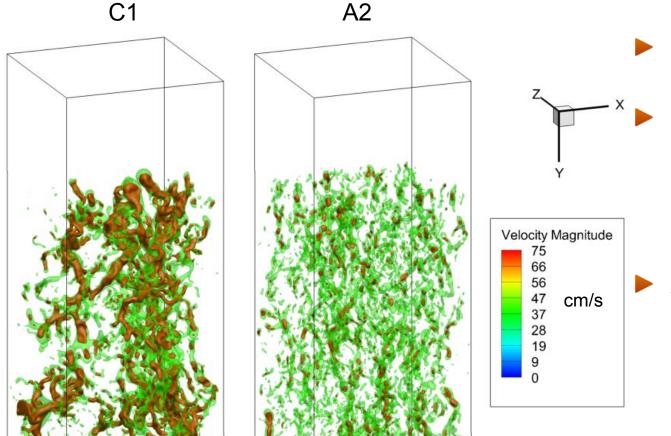
75.0 cm/s

### Technical accomplishments

#### **Lattice Boltzmann simulations**



Proudly Operated by Battelle Since 1965



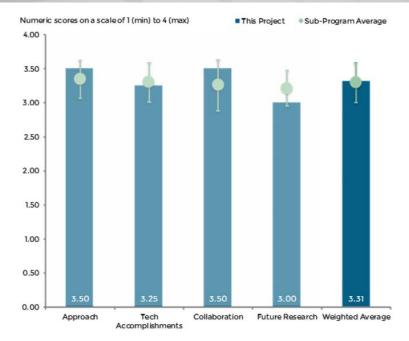
- Velocity iso-surfaces at 75, 40 cm/s
- Smaller high-velocity regions are more distributed throughout the wall volume in A2
- At these thresholds, some of the largest, twisting paths through portions of the C1 filter wall are visible

April 18, 2016 19

#### **FY15** reviewer comments



Proudly Operated by Battelle Since 1965



- Excellent collaboration, good communication
- These fundamental studies on gasoline particulate drivers are important to guide future direction."
- "...technical accomplishments in this area have been impressive."
- "...this project takes a comprehensive approach in characterizing the particulate matters for gasoline direct injection (GDI) engines using various fuels and at various engine operating conditions."
- "Well coupled to ACEC combustion strategies and future GDI engines"
- "Extensive work on fuel effects on in-cylinder PM formation, PM and filter characterization, and PM filtration behavior."

"...not clear to what level the experimental results have improved the feasibility or provided direction of change in the proposed model."

"Development/refinement of filter models based on test data should be pushed harder with higher priority."

Agreed. Refinement of filter models will be our top priority moving forward.

"Given the potential future application of multifunctional filter devices such as GPF and SCRF, the effects of catalyst washcoat on filtration efficiency, pressure drop, and gaseous emissions conversions need to be investigated in more detail."

Catalyzed filter samples have been procured and added to the project for filtration experiments and micro-scale characterization in FY16.

"Need to include the effects of ash on backpressure and reactivity of the soot."

Effects of ash on backpressure and filtration efficiency have been investigated over the past year in low temperature experiments. Ash will also be considered in high-temperature experiments which are commencing now.

### Collaborations



Proudly Operated by Battelle Since 1965

#### Major Partners

- General Motors Company (Industry): Provide funding (supporting full-time doctoral student working on improved models), hardware, expertise, and operational guidance for engine experiments at the ERC. Advise on project direction and priorities.
- Engine Research Center at University of Wisconsin, Madison (Academic): Operate test engine - including shakedown tests, independent experiments, and cooperative experiments. Assist in analysis and publication of data. Develop improved device-scale modeling techniques.
- Analysis subcontracts
  - Micromeritics
  - Particle Tech Labs
  - Micro Photonics

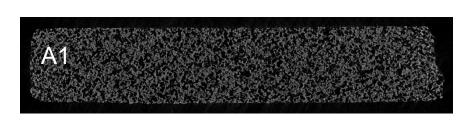
- Filter suppliers
  - Corning Incorporated
  - Ibidin
  - NGK
  - Sumitomo

### Remaining challenges and barriers



Proudly Operated by Battelle Since 1965

- Readily available characterization tools such as mercury porosimetry seem inadequate to completely describe the structural features of filters that determine performance
- ► The rich datasets available from 3-D imaging show clear differences between materials and products, but a set of quantitative, descriptive parameters that correlates directly to performance remains elusive
- More general models are needed, which will allow prediction of filter performance as a function of welldefined structural properties over a wide range of engine operating conditions
- Need filtration data for continuous regeneration conditions with little soot in the filter, representing close-coupled GPF



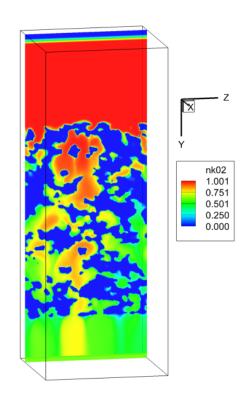


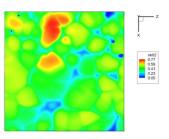
#### **Future work**



Proudly Operated by Battelle Since 1965

- Further expand set of tested filter samples, including catalyzed filter substrates
  - EFA tests
  - Micro X-Ray CT, analysis
- Test 3<sup>rd</sup> generation high-temperature sample holder/gasket system
- Perform filtration experiments representative of closecoupled filter placement
- Evaluate new porous media characterization techniques
  - Extrusion flow porometry
  - Extrusion porosimetry
- Complement experimental characterization methods with analysis of 3D micro X-Ray CT data and porescale simulations for various substrates tested
- Evaluate constricted tube filter model, comparing to experimental data
- Develop improved filtration models



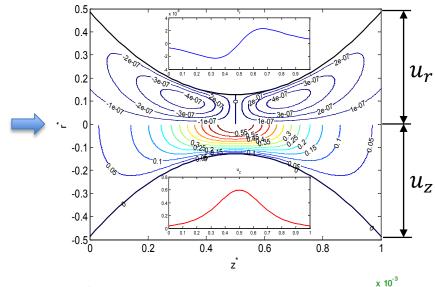


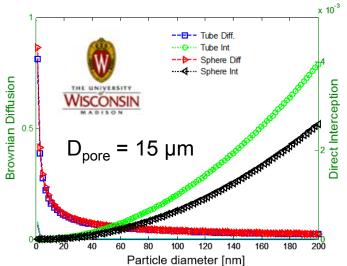
#### **Future directions**

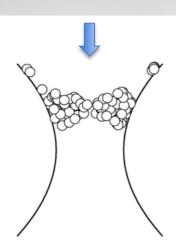
#### **Evaluation of alternative filter models**



Proudly Operated by Battelle Since 1965







- Goal is filter model that gives better predictions with minimal tuning to match data
- In addition to spherical unit collector models, other alternatives are being explored
- One candidate is the constricted tube model\*

April 18, 2016 24

<sup>\*</sup> Tien, C. and Payatakes, A., "Advances in deep bed filtration," AIChE J., no. 5, pp. 737–759, 1979.

## **Summary/Conclusions**

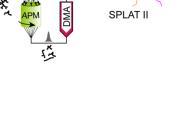


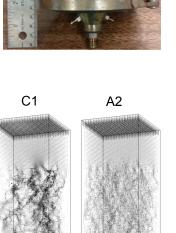
Proudly Operated by Battelle Since 1965

- Completing analysis of SIDI particulate characterization data
  - Various particle types present in exhaust in different proportions under different engine operating conditions



- Developed methods for real-time filter loading estimates from particle populations
- Evaluated effects of particle sizer scan rates on data
- Improved low temp materials/methods to avoid particle formation
- Developed 3<sup>rd</sup> generation high-temperature sample holder/gasket system
- Began building a large set of high quality fundamental filtration data
  - Evaluated sample-to-sample variation
  - Confirmed repeatability
  - Collected data for multiple substrates covering a wide range of filter properties
  - Quantified effects of low soot and ash loadings on performance
- Development of filter characterization approaches
  - Evaluating other analytical methods, including extrusion porometry and flow porosimetry
  - X-Ray CT data and micro-scale flow simulations are useful in explaining differences in substrate performance
- Exploring alternatives to standard unit collector filtration model







#### Technical Back-Up Slides

### Schedule for FY 14 cooperative experiments

22:00



Proudly Operated by Battelle Since 1965

	Monday 6/9/2014	Tuesday 6/10/2014	Wednesday 6/11/2014	New Thursday 6/12/2014	New Friday Plan 6/13/2014	Saturday 6/14/2014	Sunday 6/15/2014	Monday 6/16/2014	Tuesday 6/17/2014	Wednesday 6/18/2014 <b>E50/E100</b>	Thursday 6/19/2014	Friday 6/20/2014	
Fuel:	EEE	EEE	EEE	EEE	EEE/TRF	E10/E20/E30	E10/E20	E50/TRF/Iso	EEE/E30	ISOOCTANE	EEE	EEE	
DI / PMPV:	DI	DI	DI	PMPV	DI	PMPV	DI	PMPV	DI	DI	DI	DI	
8:00		Warmup	Warmup	Warmup	Warmup	Warmup	Warmup	Warmup	Warmup	Warmup	Warmup	Warmup	
9:00		T : 10		SOC NFB Phi = 0.98	EOI 220 Phi = 0.98	SOC NFB	EOI 220 E10 Phi = 0.98	SOC NFB E50 Phi = 0.98	Sandeep Tests	EOI 220 E50 Phi = 0.98		Probing C1, Heavy Load,	
10:00	Trial Run	Trial Run	EOI 220	SOC - Low DR	EOI 340	E10 Phi = 0.98	EOI 190	SOC	EOI 220	EOI 280	Heavy	Filtration	
				Phi = 1.50	Phi = 0.98	SOC	E10 Phi = 0.98	E50 Phi = 1.63	EEE Phi = 0.98	E50 Phi = 0.98		Probing	
11:00		EOI 220 Characterizatio n		High Load	EOI 250 (min part)	E10 Phi = 1.43	EOI 250	SOC	EOI 310	EOI 250		Filtration	
				Troubleshoot	Phi = 1.50	Phi = 0.98	soc	E10 Phi = 0.98	E50 Phi = 1.56	EEE Phi = 0.98	E50 Phi = 0.98		Tittation
12:00				Low Speed	EOI 140	E10 Phi = 1.50	EOI 280	Change Fuel	EOI 190	EOI 190		Probing	
		Rich		Phi = 1.50	Phi = 0.98	Change Fuel	E10 Phi = 0.98	SOC NFB	EEE Phi = 0.98	E50 Phi = 0.98	4		
13:00		Characterizatio n		SOC - Low DR	EOI 220 - Random Fire	SOC NFB	EOI 310	TRF Phi = 0.98	EOI 280	EOI 310		Filtration	
	Setup			Phi = 0.98	Phi = 0.98	E20 Phi = 0.98	E10 Phi = 0.98	SOC	EEE Phi = 0.98	E50 Phi = 0.98		Probing	
14:00	&	EOI 280	EOI 220	High Load	Change Fuel	SOC	Change Fuel	TRF Phi = 1.50	EOI 250	Change Fuel			
	Troubleshoot	Characterizatio n	Characterizatio n	Phi = 1.40	EOI 220	E20 Phi = 1.46	EOI 220	SOC	EEE Phi = 0.98	EOI 220	Probing		
15:00				SOC	TRF Phi = 0.98	SOC	E20 Phi = 0.98	TRF Phi = 1.40		E100 Phi = 0.98	through Bypass		
		MBT -15	64 501000	Phi = 1.40	EOI 340	E20 Phi = 1.52	EOI 250	SOC	EOI 220	EOI 190	and Clean Filter		
16:00		Characterizatio n	n Filtration	Low Speed	TRF Phi = 0.98	Change Fuel	E20 Phi = 0.98	TRF Phi = 1.35	E30 Phi = 0.98	E100 Phi = 0.98		Packing	
			(Wash 15)	Phi = 1.40	EOI 250 (min part)		EOI 280	Change Fuel	EOI 310	EOI 250			
17:00		EFA		SOC SPIKE	TRF Phi = 0.98	SOC NFB	E20 Phi = 0.98	SOC NFB		E100 Phi = 0.98			
		Troubleshoot	EFA .	Phi = 1.35	EOI 140	E30 Phi = 0.98	EOI 190	ISO Phi = 0.98	EOI 190	EOI 280	Filtration		
18:00			Troubleshoot	SOC Normal	TRF Phi = 0.98	SOC	E20 Phi = 0.98	SOC		E100 Phi = 0.98	Probing		
19:00			Heavy Load	Phi = 1.35		E30 Phi = 1.50 SOC	EOI 310 E20 Phi = 0.98	ISO Phi = 1.50	EOI 280	EOI 310 E100 Phi = 0.98	Filtration		
19.00			Characterizatio			E30 Phi = 1.55	EOI 220		EOI 250	EOI 220	Probing		
20:00			n C2, Cold		ļ		E20 Phi = 0.98		F30 Phi - 0 09	E100 Phi = 0.98		I	
20.00			probing				LZUTIII - 0.96	I	EOI 220	L1001111 - 0.98	J		
21:00			Proping						E30 Phi = 0.98				
										1			

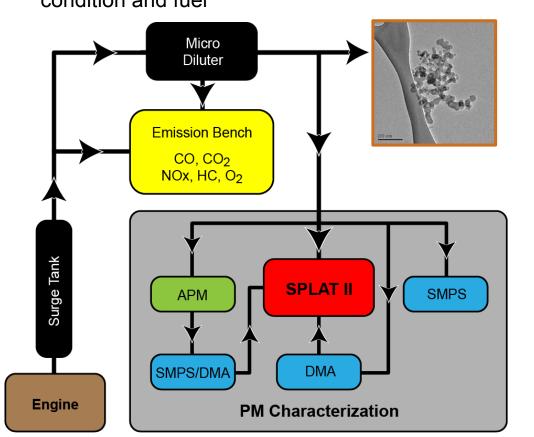
### **Approach**



Proudly Operated by Battelle Since 1965

- Advanced test engines at the UW ERC allow experiments with candidate next-generation gasoline engine technologies
- Highly detailed PM characterization is enabled by an array of advanced instruments and methods

Exhaust PM represents a complex mixture of particles with various sizes, shapes, morphologies, and compositions that can be identified and characterized as a function of engine operating condition and fuel



#### SMPS:

✓ size distributions (mobility), d<sub>m</sub>

#### SPLAT II:

- √ single particle size (aerodynamic), d<sub>va</sub>
- ✓ single particle composition, MS

#### DMA/SPLAT:

- $\checkmark$  effective density,  $\rho_{eff}$
- $\checkmark$  fractal dimension,  $D_{fa}$
- ✓ primary spherule diameter, d<sub>n</sub>

#### APM/DMA/SPLAT:

- √ particle mass, m<sub>p</sub>
- ✓ mass vs. mobility diameter relationship
- $\checkmark$  fractal dimensions,  $D_{fm}$ ,  $D_{pr}$
- ✓ primary spherule diameter, d<sub>n</sub>
- $\checkmark$  number of spherules,  $N_p$
- ✓ void fraction, Φ
- ✓ dynamic shape factors  $(\chi_{t}, \chi_{v})$

√ real-time shape-based separation

# **Exhaust Filtration Analysis (EFA) experiments**



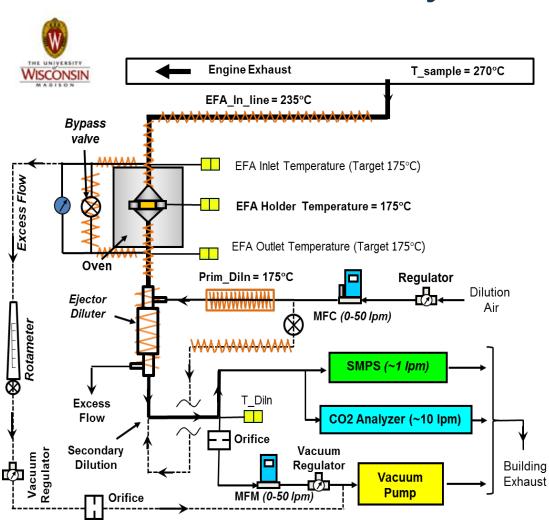
Proudly Operated by Battelle Since 1965

#### **GM / UW-Madison Collaborative Research Laboratory**



- Filtration experiments conducted with flat wafer samples and exhaust from single cylinder test engine
- Particulates measured with Scanning Mobility Particle Sizer (SMPS) and Engine Exhaust Particle Sizer (EEPS)

See SAE-2014-01-1558



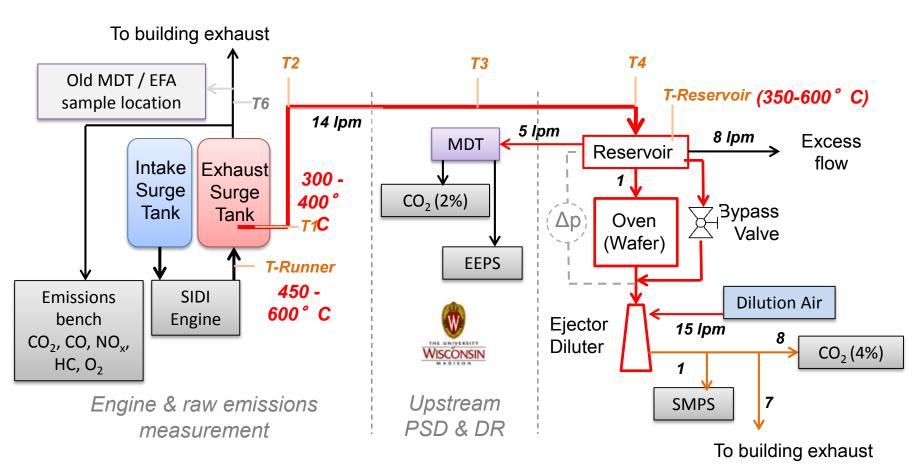
### **EFA Modifications**

### **High temperature setup**



Proudly Operated by Battelle Since 1965

#### **GM / UW-Madison Collaborative Research Laboratory**



 Impact of modified setup & sampling location on PSD was relatively small

Filtration, downstream PSD & DR

# Heterogeneous Multi-scale Filtration (HMF) model



Proudly Operated by Battelle Since 1965

#### **GM / UW-Madison Collaborative Research Laboratory**

- Mean collector size (standard approach)
  - Mean pore size and mean porosity

$$\eta_{mean}(dp_i) = 1 - \exp\left(-\frac{3*\eta_{comb}(dp_i, dc_{mean})*(1-\epsilon_{mean})*w}{2*\epsilon_{mean}*dc_{mean}}\right)$$



- Use a cluster of collectors with different diameters to represent the complex porous structure
- Pore size PDF and porosity distribution

$$\eta_i(dp_i, \frac{dc_i}{dc_i}) = 1 - \exp\left(-\frac{3*\eta_{comb}(dp_i, dc_i)*(1-\epsilon_j)*w}{2*\epsilon_j*dc_i}\right)$$

$$\eta_{HMF}(dp_i) = \frac{\int \eta_i(dp_i, dc_i) \cdot dc_i^2 \cdot pdf(dc_i) d(dc_i)}{\int pdf(dc_i) \cdot dc_i^2 d(dc_i)}$$



